

The local Nusselt number at a location  $x$  for laminar flow over a flat plate

Laminar:  $Nu_x = \frac{h_x x}{k} = 0.332 Re_x^{0.5} Pr^{1/3}$   $Pr > 0.6, Re_x < 5 \times 10^5$

Turbulent:  $Nu_x = \frac{h_x x}{k} = 0.0296 Re_x^{0.8} Pr^{1/3}$   $0.6 \leq Pr \leq 60$   
 $5 \times 10^5 \leq Re_x \leq 10^7$

**ME313 Heat Transfer  
Formula Sheet Exam 2**

$R = 0.287 \text{ kJ/kg K}$

$(T_{m-1} - 2T_m + T_{m+1}) / \Delta x^2 = 0$  (no heat generation)

$Nu = \frac{hL_c}{k}$

$St = \frac{h}{\rho c_p V} = \frac{Nu}{Re_L Pr}$

$F_f = C_f A_s \frac{\rho V^2}{2}$

$\tau_w = \mu \left. \frac{\partial u}{\partial y} \right|_{y=0}$  or  $\tau_w = C_f \frac{\rho V^2}{2}$

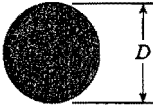
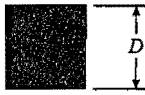


$C_{f,x} \frac{Re_L}{2} = Nu_x$  (Pr = 1)

$C_{f,x} \frac{Re_L}{2} = Nu_x Pr^{-1/3}$  or  $\frac{C_{f,x}}{2} = \frac{St_x Pr^{2/3}}$

$h = \frac{C_f \rho V c_p}{2 Pr^{2/3}}$

**TABLE A-14**

Empirical correlations for the average Nusselt number for forced convection over circular and noncircular cylinders in cross flow (from Zukauskas, 1972 and Jakob, 1949)

Cross-section of the cylinder	Fluid	Range of Re	Nusselt number
Circle 	Gas or liquid	0.4-4 4-40 40-4000 4000-40,000 40,000-400,000	$Nu = 0.989 Re^{0.330} Pr^{1/3}$ $Nu = 0.911 Re^{0.385} Pr^{1/3}$ $Nu = 0.683 Re^{0.466} Pr^{1/3}$ $Nu = 0.193 Re^{0.618} Pr^{1/3}$ $Nu = 0.027 Re^{0.805} Pr^{1/3}$
Square 	Gas	5000-100,000	$Nu = 0.102 Re^{0.675} Pr^{1/3}$
Square (tilted 45°) 	Gas	5000-100,000	$Nu = 0.246 Re^{0.588} Pr^{1/3}$
Hexagon 	Gas	5000-100,000	$Nu = 0.153 Re^{0.638} Pr^{1/3}$

**TABLE A-15**

Properties of air at 1 atm pressure

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr
-150	2.866	983	0.01171	$4.158 \times 10^{-6}$	$8.636 \times 10^{-6}$	$3.013 \times 10^{-6}$	0.7246
-100	2.038	966	0.01582	$8.036 \times 10^{-6}$	$1.189 \times 10^{-5}$	$5.837 \times 10^{-6}$	0.7263
-50	1.582	999	0.01979	$1.252 \times 10^{-5}$	$1.474 \times 10^{-5}$	$9.319 \times 10^{-6}$	0.7440
-40	1.514	1002	0.02057	$1.356 \times 10^{-5}$	$1.527 \times 10^{-5}$	$1.008 \times 10^{-5}$	0.7436
-30	1.451	1004	0.02134	$1.465 \times 10^{-5}$	$1.579 \times 10^{-5}$	$1.087 \times 10^{-5}$	0.7425
-20	1.394	1005	0.02211	$1.578 \times 10^{-5}$	$1.630 \times 10^{-5}$	$1.169 \times 10^{-5}$	0.7408
-10	1.341	1006	0.02288	$1.696 \times 10^{-5}$	$1.680 \times 10^{-5}$	$1.252 \times 10^{-5}$	0.7387
0	1.292	1006	0.02364	$1.818 \times 10^{-5}$	$1.729 \times 10^{-5}$	$1.338 \times 10^{-5}$	0.7362
5	1.269	1006	0.02401	$1.880 \times 10^{-5}$	$1.754 \times 10^{-5}$	$1.382 \times 10^{-5}$	0.7350
10	1.246	1006	0.02439	$1.944 \times 10^{-5}$	$1.778 \times 10^{-5}$	$1.426 \times 10^{-5}$	0.7336
15	1.225	1007	0.02476	$2.009 \times 10^{-5}$	$1.802 \times 10^{-5}$	$1.470 \times 10^{-5}$	0.7323
20	1.204	1007	0.02514	$2.074 \times 10^{-5}$	$1.825 \times 10^{-5}$	$1.516 \times 10^{-5}$	0.7309
25	1.184	1007	0.02551	$2.141 \times 10^{-5}$	$1.849 \times 10^{-5}$	$1.562 \times 10^{-5}$	0.7296
30	1.164	1007	0.02588	$2.208 \times 10^{-5}$	$1.872 \times 10^{-5}$	$1.608 \times 10^{-5}$	0.7282
35	1.145	1007	0.02625	$2.277 \times 10^{-5}$	$1.895 \times 10^{-5}$	$1.655 \times 10^{-5}$	0.7268
40	1.127	1007	0.02662	$2.346 \times 10^{-5}$	$1.918 \times 10^{-5}$	$1.702 \times 10^{-5}$	0.7255
45	1.109	1007	0.02699	$2.416 \times 10^{-5}$	$1.941 \times 10^{-5}$	$1.750 \times 10^{-5}$	0.7241
50	1.092	1007	0.02735	$2.487 \times 10^{-5}$	$1.963 \times 10^{-5}$	$1.798 \times 10^{-5}$	0.7228
60	1.059	1007	0.02808	$2.632 \times 10^{-5}$	$2.008 \times 10^{-5}$	$1.896 \times 10^{-5}$	0.7202
		1007	0.02881	$2.780 \times 10^{-5}$	$2.052 \times 10^{-5}$	$1.995 \times 10^{-5}$	0.7177
					$2.096 \times 10^{-5}$	$2.097 \times 10^{-5}$	0.7154